

GUJARAT TECHNOLOGICAL UNIVERSITY**BE - SEMESTER-VI (NEW) EXAMINATION – SUMMER 2022****Subject Code:3161911****Date:06/06/2022****Subject Name:Design of Heat exchangers****Time:10:30 AM TO 01:00 PM****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Simple and non-programmable scientific calculators are allowed.

MARKS

Q.1 (a) In what way Boiling & Condensation differs from other types of heat exchange? **03**

(b) Double tube counter flow heat exchanger is used to cool hot oil. The Copper inner tube have a diameter of 2 cm and negligible thickness. The inner diameter of outer tube (shell) is 3 cm. Water flows through outer tube at the rate of 0.5 kg/sec and oil through outer shell at rate of 0.8 kg/sec. Taking average temperature of water and oil to be 45°C and 80°C respectively. Calculate Inner side heat transfer coefficient using given properties. **04**

Use Dittus Boelter equation for turbulent flow

$$Nu = 0.023 (Re)^{0.8} (Pr)^{0.4}$$

Properties (Unit)	Water
Density (kg/m ³)	990.1
Thermal Conductivity (W/m K)	0.637
Viscosity (m ² /s)	0.602 x 10 ⁻⁶
Prandtl number (-)	3.91

(c) What is fouling in heat exchanger? Discuss its effect on heat transfer and pressure drop. **07**

Q.2 (a) What is the correction factor? When it is used in heat exchanger? **03**

(b) List out the main selection criteria of a heat exchanger. State requirements of good heat exchangers. **04**

- (c) Water at a flow rate of 5000 kg/h will be heated from 20 to 35°C by hot water at 140 °C. A 15 °C hot water temperature drop is allowed. A number of 1.5 m hairpins of 3 in (annulus inner diameter, $D_i = 0.0779$ m) by 2 in (inner tube $d_o = 0.0603$ m and $d_i = 0.0525$ m) double pipe heat exchangers with annuli and pipes each connected in series will be used. Hot water flows through inner tube. Fouling factors are $R_i = 0.000176$ m²-K/W and $R_o = 0.000352$ m²-K/W. Assume that pipe is made of carbon steel ($k = 54$ W/m-K). Calculate: (1) Heat transfer coefficient for the fluid flowing through inner tube and annulus (2) The number of hairpins required. Use following properties data and correlation for calculation.

Correlation:

$$Nu_b = \frac{\left(\frac{f}{2}\right)(Re_b)Pr_b}{1 + 8.7\left(\frac{f}{2}\right)^{0.5}(Pr_b - 1)}$$

$$f = (1.58 \ln Re - 3.28)^{-2} \text{ for Inner tube}$$

$$f = (3.64 \log_{10} Re - 3.28)^{-2} \text{ for annulus}$$

Properties (Unit)	Inner Tube	Annulus
Density (kg/m ³)	932.53	996.4
Specific heat (kJ.kg K)	4.268	4.179
Thermal Conductivity (W/m K)	0.687	0.609
Dynamic viscosity (Pa S)	0.207×10^{-3}	0.841×10^{-3}
Prandtl number (-)	1.28	5.77

OR

- (c) In an open heart surgery under hypothermic conditions, the patient's blood is cooled before the surgery and rewarded afterwards. It is proposed that a concentric tube counter flow heat exchanger of length 0.5m is to be used for this purpose with a thin walled inner tube having a diameter of 55mm. If water at 60°C and 0.1kg/s is used to heat blood entering the heat exchanger at 18°C and 0.05kg/s, what is the temperature of blood leaving the heat exchanger and the heat flow rate. Take $U_o = 500$ W/m²K, c_p of blood = 3.5 kJ/kg K and c_p of water = 4.183 kJ/kg K.

- Q.3** (a) Derive expression for hydraulic and equivalent diameter for hairpin heat exchanger. 03
- (b) Feed water heater of a steam generator is in the form of a single pass, shell and tube heat exchanger consisting of 100 tubes (25mm ID, 31mm OD). 500 Lpm of water is heated from 30°C to 70°C by condensing steam at standard atmosphere pressure on shell side. The shell side heat transfer coefficient is 5000W/m²K. On waterside, heat transfer coefficient is 1270W/m²K and fouling factor is 0.0002m²K/W. Neglect fouling factor on shell side and resistance offered by tube wall. Calculate the required length of the tubes. 04
- (c) Explain the procedure of calculating total pressure drop in double pipe heat exchanger. 07

OR

- Q.3** (a) Consider two double pipe counterflow heat exchangers that are identical except that one is twice as long as the other one. Which of the exchangers is more likely to have a higher effectiveness? **03**
- (b) What is the effect in design of heat exchanger when **04**
- 1) Pressure drop on the tube side is greater than allowable pressure drop?
 - 2) Shell side pressure drop is greater than allowable pressure drop?
- (c) A 3 m long Shell and tube heat exchanger which is designed to heat raw water by the use of condensed water at 67°C and 0.2 bar, which will flow in the shell side with a mass flow rate of 50,000 kg/hr. The heat will be transferred to 30,000 kg/hr of city water coming from a supply at 17°C ($c_p = 4184 \text{ J/kg K}$). A single shell and a single tube pass is preferable. A fouling resistance of $0.000176 \text{ m}^2 \text{ K /W}$ is suggested and the surface over design should not be over 40 %. A maximum coolant velocity of 1.5 m/s is suggested to prevent erosion. A maximum tube length of 5 m is required because of space limitations. The tube material of carbon steel ($k=60 \text{ W/m K}$). Raw water will flow inside straight tubes whose outer diameter is 19 mm and inner diameter is 16 mm. Tubes are laid out on a square pitch with a pitch ratio of 1.25. The baffle spacing is approximated by 0.6 of shell diameter and the baffle cut is set to 25%. The water outlet temperature should not be less than 40°C. Consider shell side heat transfer coefficient $5000 \text{ W/m}^2 \text{ K}$, tube side it is $4000 \text{ W/m}^2 \text{ K}$, correction factor 0.90 and tube calculation constant $CTP = 0.93$ and $CL = 1$. Calculate:
- 1) Outlet temperature of hot fluid
 - 2) Overall surface design
 - 3) Shell diameter
 - 4) Number of tubes
- Q.4** (a) If we have to process a corrosive liquid in a heat exchanger, where will you prefer to send it, tube-side or shell-side of the heat exchanger. Support your answer with the reasoning. **03**
- (b) Draw the diagram for following tube arrangement in shell and tube heat exchanger: **04**
- 1) Equilateral triangle
 - 2) Square
 - 3) Rotated square
- Compare them in terms of tube density, heat transfer coefficient and fouling liquid (mechanical cleaning).
- (c) Air enters the core of a finned-tube heat exchanger of the type shown in Figure 1 at 1 atm and 30°C. The air flows at a rate of 1,500 kg/h perpendicular to the tubes and exits with a mean temperature of 100°C. The core is 0.5 m long with a 0.25 m^2 frontal area. The air densities at the inlet and outlet are 1.177 and 0.954 kg/m^3 . The properties of air at bulk temperatures are density = 1.038 kg/m^3 , $Pr = 0.719$, viscosity = $2.04 \times 10^{-5} \text{ kg/m s}$ and specific heat 1.007 kJ/kg K . Calculate the total pressure drop between the air inlet and outlet and the average heat transfer coefficient on the air side for friction factor 0.057. **07**
- OR**
- Q.4** (a) What is the heat capacity rate? What can you say about the temperature changes of the hot and cold fluids in heat exchangers if both fluids have the same capacity? **03**

- (b) Explain the effect of following parameter on heat transfer and pressure drop. **04**
- 1) Number of tubes at tube side
 - 2) Baffle spacing at shell side
 - 3) Baffle cut at shell side
 - 4) Tube pitch at shell side

- (c) In a compact heat exchanger, air at 2 atm and 500 K with the velocity (u_∞) of 20 m/s flow across a compact heat exchanger matrix (where ratio of minimum free-flow area to frontal area is 0.78). Calculate 1) the heat transfer coefficient and 2) the frictional pressure drop. Length of the matrix is 0.8 m. Take $\rho = 1.41 \text{ kg/m}^3$, $D_h = 0.3434 \times 10^{-2} \text{ m}$, $C_p = 1030 \text{ J/kg.K}$, $\mu = 2.69 \times 10^{-5} \text{ kg/m.s}$ and $Pr = 0.718$. Refer given table for appropriate property selection. **07**

Effect of Reynolds number on heat transfer and pressure drop

characteristics			
Re	$\frac{h}{G C_p} Pr^{2/3}$	f	Density Ratio at Inlet and Outlet
3000	0.0040	0.012	0.8
4000	0.0045	0.018	0.9
4500	0.0056	0.023	1.0
5000	0.0065	0.030	1.0

- Q.5** (a) Why compact heat exchangers are more suitable for gaseous fluid? **03**

- (b) When is a heat exchanger classified as being compact? Name the specific exchanger construction type that may be used in the following applications: (a) Air Preheater (b) Automotive Radiator (c) Condenser of an air conditioner. **04**

- (c) What is the use of pinch analysis. Explain its principal taking reference of hot and cold stream. **07**

OR

- Q.5** (a) What is the use of tie rods and spacers in shell-and-tube heat Exchangers ? **03**

- (b) List out different application for plate type heat exchanger and explain its advantages and disadvantages over other heat exchanger. **04**

- (c) Enlist different active and passive technique for heat transfer enhancement. What is the effect of following parameter on heat transfer performance? **07**

- 1) Coated surface
- 2) Surface roughness
- 3) Extended surface
- 4) Displaced insert
- 5) Swirl flow
- 6) Coiled tubes
- 7) Additives for liquid and gases

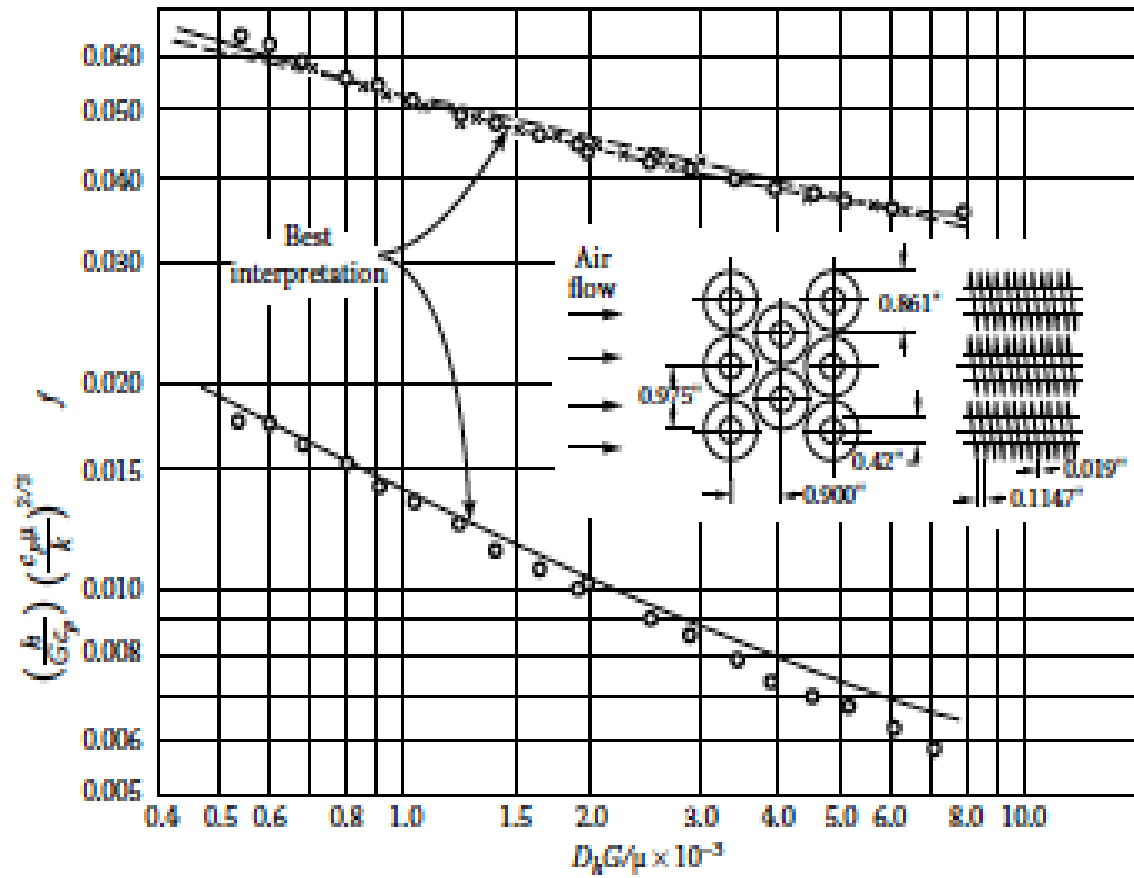


Figure 1. Heat transfer and friction factor for flow across circular finned-tube matrix. Surface CF-8.72(c): tube OD = 1.07 cm; fin pitch = 3.43/cm; fin thickness = 0.048 cm; fin area/total area = 0.876; air passage hydraulic diameter, $d_h = 0.443$ cm; free-flow area/frontal area, $\sigma = 0.494$; heat transfer area/total volume = 446 m^2/m^3 .
