

GUJARAT TECHNOLOGICAL UNIVERSITY

BE - SEMESTER-IV (NEW) EXAMINATION – SUMMER 2024

Subject Code:3140503

Date:18-07-2024

Subject Name: Heat Transfer

Time:10:30 AM TO 01:00 PM

Total Marks:70

Instructions:

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Simple and non-programmable scientific calculators are allowed.

	MARKS
Q.1 (a) List out features of unit operations. Also Define Heat transfer.	03
(b) A furnace is constructed with 225 mm thick of fire brick, 120 mm of insulating brick and 225 mm of building brick. The inside temperature is 1200 K and the outside temperature is 330 K. Find the heat loss per unit area and the temperature at the junction of the fire and insulating brick. Data: k for fire brick = 1.4 W/(m.K) , k for insulating brick = 0.2 W/(m.K) , k for building brick = 0.7 W/(m.K)	04
(c) Why Insulation is necessary for process equipment. Also Mention characteristics of insulating material & Derive equation for critical radius of insulation.	07
Q.2 (a) Discuss the Physical significance of (i) Prandtl Number (ii) Peclet Number (iii) Biot Number.	03
(b) Explain Velocity boundary layer & Thermal boundary layer. Which dimensionless number is related to it? How?	04
(c) Determine the heat transfer coefficient for water flowing in a tube of 16 mm diameter at a velocity of 3 m/s. The temperature of the tube is 297 K and the water enters at 353 K and leaves at 309 K. Using Dittus-Boelter equation and Sieder-Tate equation. Data : Properties of water at 331 K at arithmetic mean-bulk temperature are: $\rho = 984.1 \text{ kg/m}^3$, $C_p = 4187 \text{ J/(kg.K)}$, $\mu = 485 \times 10^{-6} \text{ Pa.s}$, $k = 0.657 \text{ W/(m.K)}$, Viscosity of water at 297 K, $\mu_w = 920 \times 10^{-6} \text{ Pa.s}$	07
OR	
(c) Derive the equation of overall heat transfer co-efficient(U) from the individual heat transfer co-efficient(h) with neat sketch.	07
Q.3 (a) Define: Thermal Conductivity. Enlist the factors on which thermal conductivity of a substance depends?	03
(b) Describe any two laws of black body radiation.	04
(c) What is boiling and when does it occurs? Explain Nucleate boiling.	07

OR

Q.3	(a)	Explain basic law for heat conduction.	03
	(b)	Explain Kirchhoff's law and Total emissive power for radiation.	04
	(c)	Define Condensation. Explain filmwise condensation & Dropwise condensation.	07
Q.4	(a)	Define: Tube Pitch, Baffle Spacing & Range.	03
	(b)	What do you mean by "fouling" in heat exchangers? What is the effect of it on performance of heat exchangers?	04
	(c)	Explain design steps for Shell & Tube heat exchanger in detail. Draw neat sketch of 2-4 pass shell & tube heat exchanger.	07
OR			
Q.4	(a)	Define Fin. Enlist different types of it. Differ Transverse fin with longitudinal fin.	03
	(b)	What are the advantages of square pitch arrangement over the triangular pitch in case of heat exchanger tubes?	04
	(c)	With neat diagram explain construction and working of falling film evaporator.	07
Q.5	(a)	Explain the significance of LMTD correction factor.	03
	(b)	Explain Boiling Point Elevation (BPE).	04
	(c)	What is importance of LMTD? Derive the equation for parallel flow arrangement.	07
OR			
Q.5	(a)	Define Capacity and Economy of evaporator.	03
	(b)	Calculate rate of heat loss from a thermoflask if the polished silvered surfaces have emissivities of 0.05, the liquid in the flask is at 368 K and the casing is at 293 K. Calculate loss if both surfaces were black. Stefan Boltzmann constant = $5.67 \times 10^{-8} \text{ W}/(\text{m}^2 \cdot \text{K}^4)$	04
	(c)	Write a short note on Multiple Effect Evaporator.	07
