

Seat No.: \_\_\_\_\_

Enrolment No. \_\_\_\_\_

## GUJARAT TECHNOLOGICAL UNIVERSITY

BE - SEMESTER-V (NEW) EXAMINATION – WINTER 2023

Subject Code: 3150501

Date: 07-12-2023

Subject Name: Mass Transfer Operations I

Time: 10:30 AM TO 01:00 PM

Total Marks: 70

**Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Simple and non-programmable scientific calculators are allowed.

- Q.1**
- (a) Explain film theory for mass transfer coefficient. **03**
  - (b) Differentiate between packed towers and tray tower. **04**
  - (c) Derive Fick's law of diffusion and explain  $N_A$  and  $J_A$ . Also prove that for unidirectional binary diffusion  $J_A = -J_B$ . **07**

- Q.2**
- (a) Define: (i) Flooding (ii) Priming (iii) Coning **03**
  - (b) Explain material balance for single stage extraction. **04**
  - (c) Discuss in detail classification of mass transfer operations and explain with examples. **07**

**OR**

- (c) Derive equations to calculate rate of steady state diffusion of 'A' through non-diffusing 'B' and also for steady state equimolar counter diffusion in case of gases. **07**

- Q.3**
- (a) Explain Meir's theory for crystallization. **03**
  - (b) Define (i) Weeping (ii) Dumping (iii) Tray Spacing (iv) Theoretical Tray **04**
  - (c) Ammonia and air are in equimolar counter diffusion of each other in a cylindrical tube of 3 mm diameter and 20 m length. The total pressure is 1 atm and the temperature is 25 °C. One end of the tube is connected to a large reservoir of  $\text{NH}_3$  and the other end of the tube is open to atmosphere. Estimate the mass transfer rates in kg/sec of ammonia and air. The mass diffusivity of mixture is  $0.28 \times 10^{-4} \text{ m}^2/\text{sec}$  **07**

**OR**

- Q.3**
- (a) Explain random packings and regular packing. **03**
  - (b) Explain selection criteria of solvent for gas absorption. **04**
  - (c) Explain equilateral-triangular co-ordinate, plait point, tie line, one pair partially soluble system with examples and the mixture rule. **07**

- Q.4**
- (a) Discuss construction and working of Sparged Vessel. **03**
  - (b) Discuss local and overall mass transfer coefficients. **04**
  - (c) Explain selection criteria of solvent for extraction. **07**

**OR**

- Q.4**
- (a) What is Extraction? Give the industrial applications of Extraction. **03**
  - (b) Explain mass, heat and momentum transfer analogies. **04**
  - (c) Enlist different leaching equipment and explain any one in detail with neat figure. **07**

- Q.5** (a) Explain preparation of solids for leaching. **03**  
 (b) Explain material balance for single stage leaching. **04**  
 (c) A gas mixture containing 3% by volume pentane vapour and 97 % inerts. The mixture is treated with a non-volatile absorption oil in an absorber and 97 % removal is required. The feed solvent is free from solute. The feed gas rate is 50 kmol/hr. equilibrium relation is  $Y=0.25X/(1+0.75X)$ . where Y and X are mole ratio. Calculate minimum solvent required. **07**

**OR**

- Q.5** (a) Explain diffusion in solids. **03**  
 (b) Explain construction and working agitated tank crystallizer with the help of a neat sketch. **04**  
 (c) 5000 kg/hr of a SO<sub>2</sub>-air mixture containing 5% by volume of SO<sub>2</sub> is to be scrubbed with 2,00,000 kg/hr of water in a packed tower. The exit concentration of SO<sub>2</sub> is reduced to 0.15%. The tower operates at 1 atm. The equilibrium relation is given by:  $Y = 30 X$ . Y = Mole SO<sub>2</sub> / Mole air; X = Mole SO<sub>2</sub> / Mole water If the packed height of tower (Z) is 0.42 m, Calculate the height of transfer unit (HTU). **07**

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