

GUJARAT TECHNOLOGICAL UNIVERSITY**BE – SEMESTER- V EXAMINATION-SUMMER 2023****Subject Code: 3150501****Date: 26/06/2023****Subject Name: Mass Transfer Operations I****Time: 02:30 PM TO 05:00 PM****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Simple and non-programmable scientific calculators are allowed.

MARKS

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| Q.1 | (a) Define: 1) Mass Transfer 2) Equilibrium 3) Mass transfer Co-efficient | 03 |
| | (b) Define molecular diffusion. Derive the equation for steady state diffusion of liquid A through non diffusing liquid B. | 04 |
| | (c) Derive the equation which shows relationship between overall mass transfer coefficients (represented by K_y and K_x) and individual mass transfer coefficients (represented by k_y and k_x) with neat diagram. | 07 |
| | | |
| Q.2 | (a) State Fick's law of diffusion and prove that $D_{AB} = D_{BA}$. | 03 |
| | (b) Explain the concept of penetration theory with neat sketch and suitable assumptions. | 04 |
| | (c) Alcohol vapor is being absorbed from a mixture of alcohol vapor and water vapor by means of a nonvolatile solvent in which alcohol is soluble but water is not. The temperature is 97°C and the total pressure is 760 mm Hg. The alcohol vapor can be considered to be diffusing through a film of alcohol-water-vapor mixture 0.1 mm thick. The mole % of alcohol in the vapor at the outside of the film is 80%, and that on the inside, next to the solvent is 10%. The diffusivity of alcohol-water-vapor mixture at 25°C and 1 atm is $0.15\text{ cm}^2/\text{sec}$. Calculate the rate of diffusion of alcohol vapor in kg per hour if the area of the film is 10 m^2 . Molecular weight of Alcohol = 46 g/mol | 07 |
| OR | | |
| | (c) At 293 K solubility of ammonia in water is given by Henry's law $p=0.3672 C$, where p is in atmosphere and C is in kmol/m^3 . A mixture of 15 % ammonia and 85 % air by volume at 1 atm is in contact with an aqueous solution containing 0.147 gmol/lit. The air velocity is such that $k_G/k_L=0.9$. Find the concentration of ammonia and partial pressure at interface. | 07 |
| | | |
| Q.3 | (a) Explain the solvent selection criteria for Absorption. | 03 |
| | (b) Give stepwise procedure for determining minimum liquid to gas ratio for absorbers. | 04 |
| | (c) An air- NH_3 mixture containing 5% NH_3 is being scrubbed with water in a packed tower to recover 95% NH_3 . $G_1=3000\text{ kg/h m}^2$, $L_s=2500\text{ kg/h m}^2$. Tower is maintained at 25°C and 1 atm pressure. Find NTU and height of the tower. The equilibrium relation is given by $y^*=0.98x$, where x and y are mole fraction units. $K_{Ga}=65\text{ kmol/h m}^3\text{ atm}$. | 07 |
| OR | | |
| Q.3 | (a) Define any THREE : 1) Tie-line 2) Binodal curve 3) Solutropic solution 4) Plait point | 03 |
| | (b) Deduce equation of solvent to feed ratio for single stage liquid-liquid extraction. | 04 |

- (c) Water- dioxane solution is to be separated by extraction process using benzene as solvent. At 25 °C the equilibrium distribution of dioxane between water and benzene is as follows:

07

Wt % of dioxane in water	5.1	18.9	25.2
Wt % of dioxane in benzene	5.2	22.5	32.0

At these concentrations water and benzene are substantially insoluble. 1000 kg of a 25% dioxane water solution is to be extracted to remove 95% of dioxane. The benzene is dioxane free. Calculate minimum solvent required in kg/ hr if the extraction is done in countercurrent fashion. Estimate the number of stages needed if 1.5 times the minimum amount of solvent is used.

- Q.4** (a) Define: 1) Entrainment 2) Weeping 3) Channeling 03

- (b) With neat sketch discuss Wetted wall column for gas-liquid contact operation. 04

- (c) Calculate the rate of diffusion of acetic acid (A) across a film of non-diffusing water (B) solution 2 mm thick at 17°C, when the concentration on the opposite sides of the film are 9% and 3% acid (by weight). The diffusivity of acetic acid in the solution is $0.95 \times 10^{-9} \text{ m}^2/\text{sec}$. Density of 9% and 3% by weight acid are 1012 kg/ m³ and 1003 kg/m³ respectively. 07

OR

- Q.4** (a) Explain the concept of Equilateral –Triangular Coordinates in liquid liquid extraction. 03

- (b) Explain with neat sketch the working mechanism of Ballman Extractor. 04

- (c) Differentiate between tray tower and packed tower. 07

- Q.5** (a) Mention different types of packing for gas absorption operation and their selection criterion. 03

- (b) Explain Meir's super saturation theory of crystallization with neat sketch. 04

- (c) Calculate the yield of MgSO₄*7H₂O crystals when 1000 kg saturated solution of MgSO₄ at 353 K (80°C) is cooled to 303 K (30°C), assuming 10 % of the water is lost by evaporation during cooling. 07

Solubility of MgSO₄ at 353 K (80°C) = 64.2 kg / 100 kg water

Solubility of MgSO₄ at 303 K (30°C) = 40.8 kg / 100 kg water

Atomic weight: Mg=24, S=32, O=16, H=1

OR

- Q.5** (a) Give unit of Diffusivity. How to predict the diffusivity in gases? 03

- (b) Explain mass, heat and momentum transfer analogies. 04

- (c) What is leaching? What are the industrial applications of leaching? Discuss the different types of equilibrium diagram for leaching 07
