

**GUJARAT TECHNOLOGICAL UNIVERSITY****BE - SEMESTER-VI(NEW) EXAMINATION – WINTER 2022****Subject Code:3160506****Date:14-12-2022****Subject Name:Chemical Reactions Engineering I****Time:02:30 PM TO 05:00 PM****Total Marks:70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Simple and non-programmable scientific calculators are allowed.

**MARKS**

- Q.1**
- |     |   |           |
|-----|---|-----------|
| (a) | Define rate constant. Derive the unit of rate constant. | <b>03</b> |
| (b) | Discuss the variables affecting the rate of reaction.   | <b>04</b> |
| (c) | Derive performance equation for a CSTR.                 | <b>07</b> |

- Q.2**
- |     |  |           |
|-----|--|-----------|
| (a) | Define space time, space velocity & mean residence time.   | <b>03</b> |
| (b) | Discuss in detail about Integral method and Half life Method.  | <b>04</b> |
| (c) | Discuss the analysis of total pressure data obtained in a constant volume system and establish the relation used to calculate the partial pressure of gaseous component in reaction mixture. | <b>07</b> |

**OR**

- |     |           |           |
|-----|-----------|-----------|
| (c) | Show that | <b>07</b> |
|-----|-----------|-----------|

$$\ln \frac{M - X_A}{M(1 - X_A)} = C_{A0} (M - 1) k t, M \neq 1$$

for second order irreversible bimolecular type reaction

A + B → Products with different concentration of reactants A and B.

- Q.3**
- |     |  |           |
|-----|--|-----------|
| (a) | State the points to be considered to find the size of reactor required for given duty and for a given temperature progression  | <b>03</b> |
| (b) | Discuss method of maximization of rectangles applied to find the optimum intermediate conversion and optimum sizes of two mixed flow reactors in series.   | <b>04</b> |
| (c) | An aqueous reactant stream with $C_{A0} = 4$ mol/lit passes through a mixed flow reactor followed by a plug flow reactor. The reaction is 2 <sup>nd</sup> order with respect to A. The volume of plug flow reactor is 3 times that of the mixed flow reactor. Find the concentration of A at the exit of the plug flow reactor if the concentration of A in the mixed flow reactor is 1 mol/lit. | <b>07</b> |

**OR**

- Q.3**
- |     |   |           |
|-----|---|-----------|
| (a) | Discuss fractional yield, overall yield and selectivity for parallel reaction   | <b>03</b> |
| (b) | Discuss autocatalytic reaction with conversion-time and rate concentration Curves.  | <b>04</b> |
| (c) | When elementary 2 <sup>nd</sup> order liquid reaction $2A \rightarrow 2R$ carried in a plug flow reactor, operated isothermally, with a recycle ratio of unity, conversion is found to be 66.67%. Determine the conversion if the recycle stream is shut off. | <b>07</b> |

- Q.4**
- |     |   |           |
|-----|---|-----------|
| (a) | Discuss equal sized mixed flow reactors in series         | <b>03</b> |
| (b) | Explain Plug Flow Reactors in Series and in Parallel with | <b>04</b> |

- equation.
- (c) Discuss in detailed about product distribution for parallel reaction. 07
- OR**
- Q.4** (a) Define zero order reaction with suitable example. 03
- (b) Define Overall Fractional yield and Instantaneous fractional yield for the decomposition of A into product R. 04
- (c) First order unimolecular irreversible reaction in series 07  
 $A \longrightarrow R \longrightarrow S$  takes place with specific reaction rate  $k_1$  and  $k_2$ . Express the variation of concentration of A, R and S with time. Find the expression for the time when formation of R becomes maximum.
- Q.5** (a) Define Residence Time Distribution and explain E-Curve. 03
- (b) A closed vessel has flow for which dispersion number is 0.3. We wish to represent this vessel by tanks in series model. What value of number of tanks should be selected? 04
- (c) Write a short note on equilibrium constants from thermodynamics clearly indicating the equations. 07
- OR**
- Q.5** (a) List out characteristics of good tracer 03
- (b) From the first principle prove that for a back mix reactor 04  
 (i)  $E\theta = e^{-\theta}$  and (ii)  $F\theta = 1 - e^{-\theta}$
- (c) Find out relation between conversion and temperature 07  
 (a) Between 0 °C and 100 °C determine the equilibrium conversion of A for the aqueous reaction  

$$A \rightleftharpoons B$$
 $\Delta G^\circ_{298} = -3375 \text{ cal/mol}; \Delta H^\circ_{r,298} = -18,000 \text{ cal/mol}$ 
 Plot a graph between conversion and temperature.  
 (b) What the restrictions should be placed on a reactor operating isothermally if we have to obtain fractional conversion of 75% or higher?

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